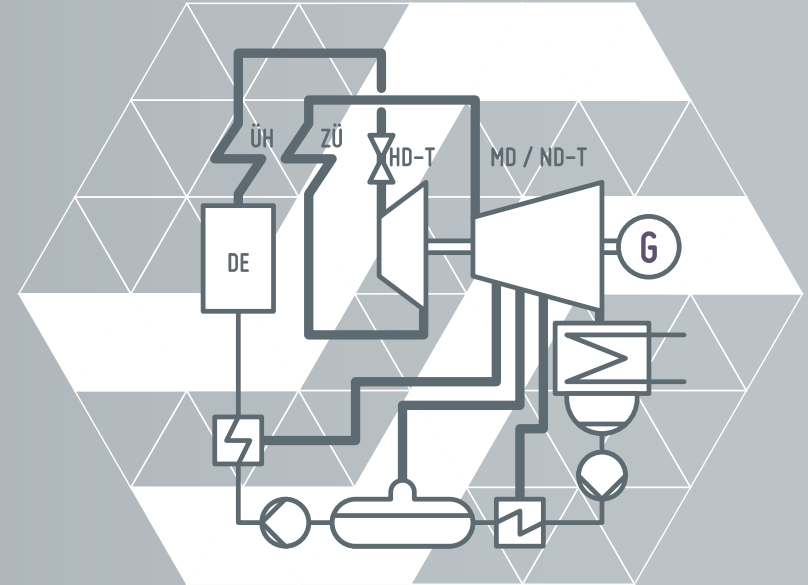


CREATING A DIGITAL TWIN OF A POWER PLANT WITH CLARA

Jan Koltermann / Sebastian Mieck
Lausitz Energie Kraftwerke Ag





01 Vorgehen Optimierung

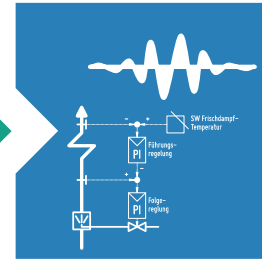
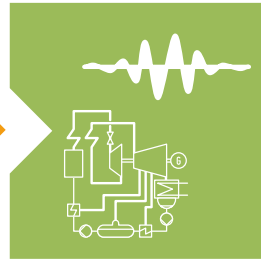
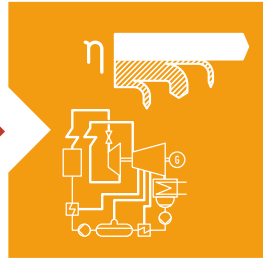
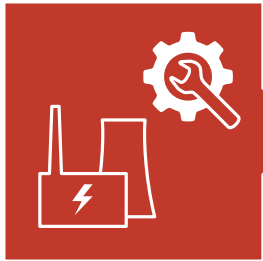
- Ausgangslage
- Themenfelder
- Herausforderungen

03 Dynamische Bewertung

- Messdatenverläufe
- Statistische Auswertung
- Wirtschaftliche Bewertung

05 Anwendung des Modells

- Szenariensimulation
- Verfahrens- und leittechnische Optimierungen
- Bewertung Lebensdauerverbrauch



02 Stationäre Bewertung

- Verteilung Prozessgrößen
- Einfluss auf Brennstoffverbrauch
- Zusammenfassung und Bewertung

04 Dynamische Modellierung

- Überblick
- Struktur Gesamtmodell
- Validierung

06 Fazit

- Zusammenfassung
- Ausblick

01 Procedure Plant optimization

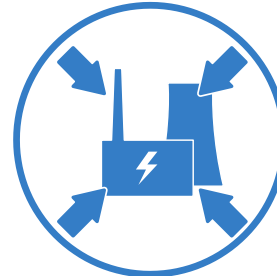
starting position



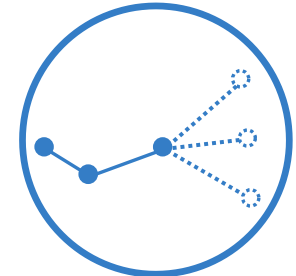
Energiewende



Fallende
Strompreise

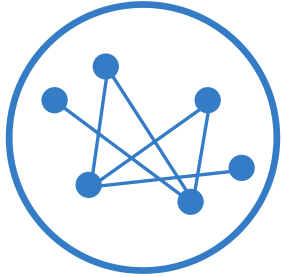


Neue
Anforderungen



Verändernde
Rahmenbedingungen &
Unsicherheiten

01 Procedure Plant optimization challenges



Hohe Komplexität
der technisch-ökonomischen
Zusammenhänge



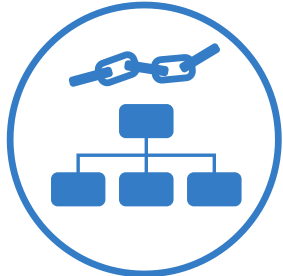
Große Datenmengen



Unvollständige
Informationen



Unterschiedliche Standpunkte &
qualitative Diskussionen



Einschränkungen aufgrund
der Organisationsstruktur



Betrieb: Fokus auf
Volllaststunden



Führung: Fokus auf
Kostensenkung



Technik: Fokus auf
Anlagenoptimierung

01 Procedure Plant optimization

Target



I. Evaluation flexibility:

- Definition of evaluation criteria
- Description Actual status
- Comparison of systems
- Comparison with the state of the art
- Identification of flexibility potentials

II. Evaluation of economic benefits:

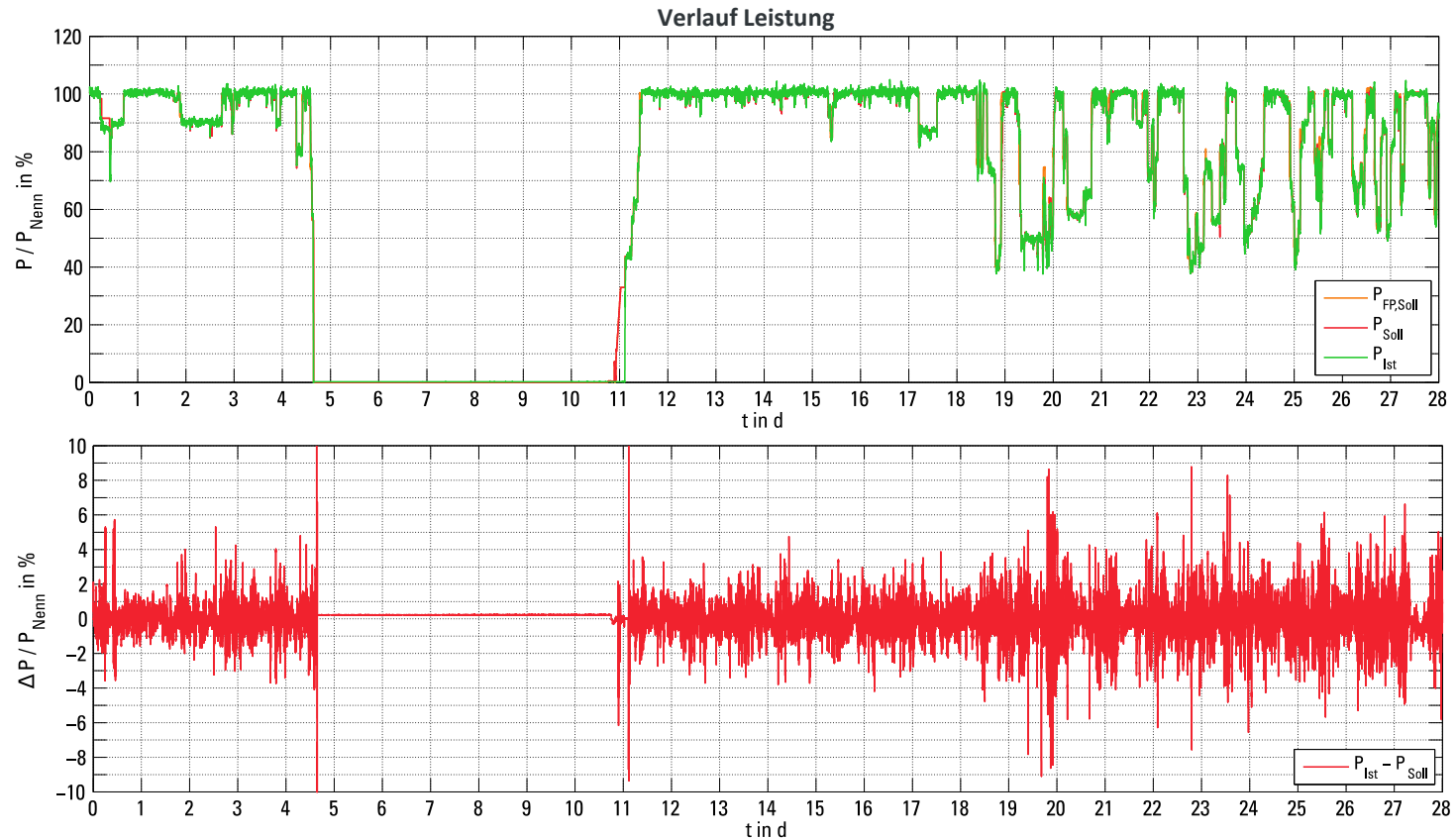
- Scenario simulations with variation of plant flexibility
- Evaluation of the driving style
- Identification of additional revenues or cost savings
- Discussion with Controlling and Power Plant Economics

III. Technical Actions:

- Development of the necessary process and I&C optimizations
- Evaluation of the adapted driving style (testing or modelling):
 - Feasibility
 - efficiency
 - control accuracy
 - Component stress (creep rupture strength and alternating fatigue))



03 Dynamic Evaluation



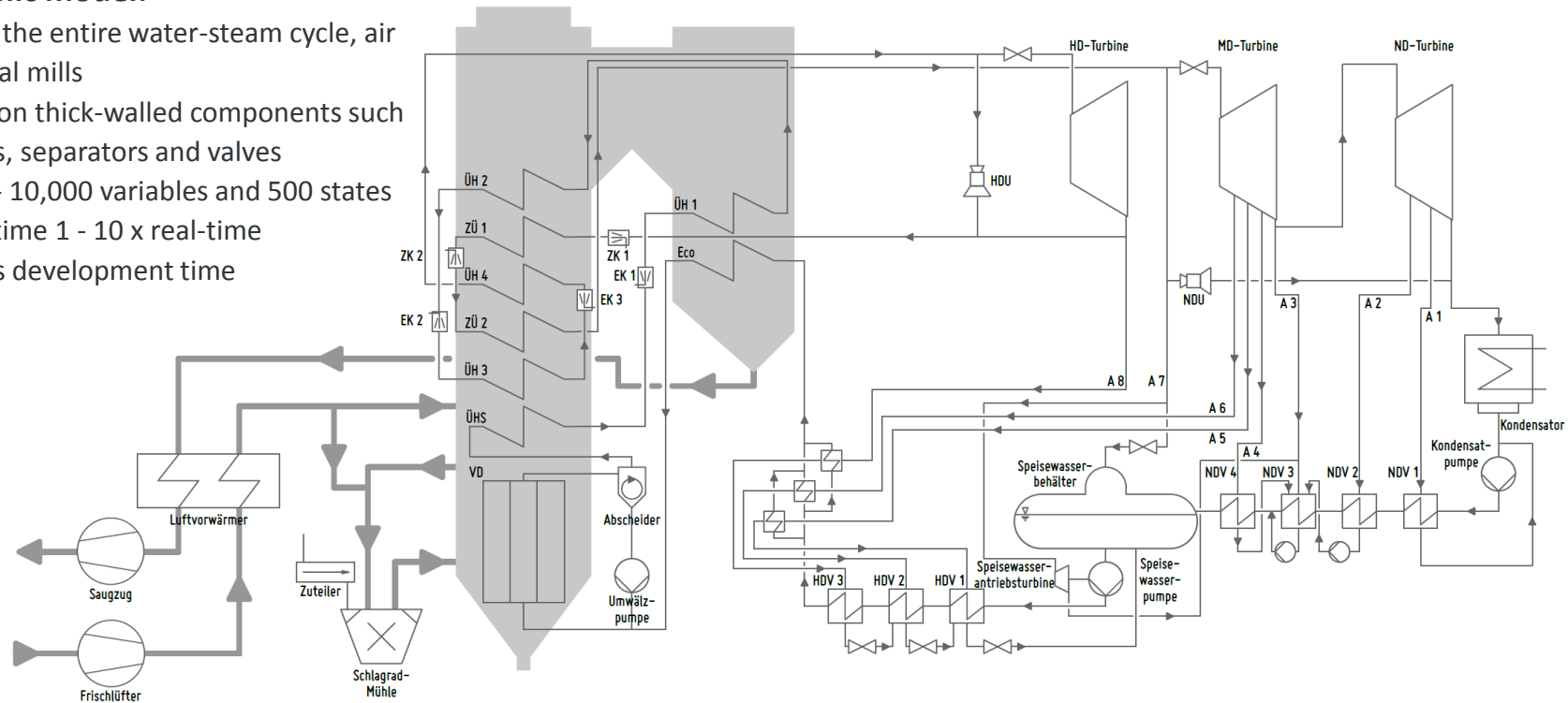
04 Dynamic power plant modelling

Model Structure



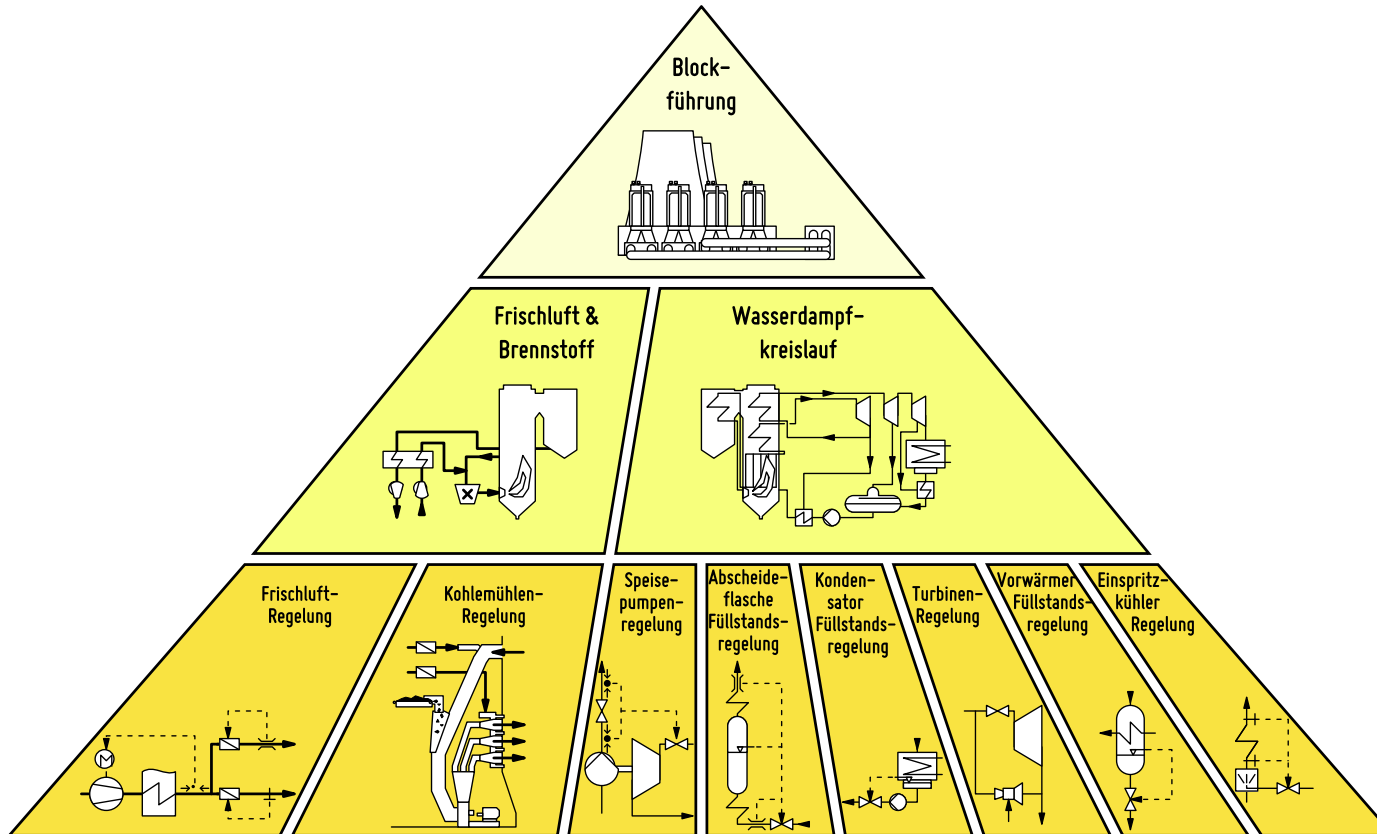
Scope dynamic model:

- Mapping of the entire water-steam cycle, air path and coal mills
- Main focus on thick-walled components such as collectors, separators and valves
- Model size - 10,000 variables and 500 states
- Simulation time 1 - 10 x real-time
- 2 man-years development time



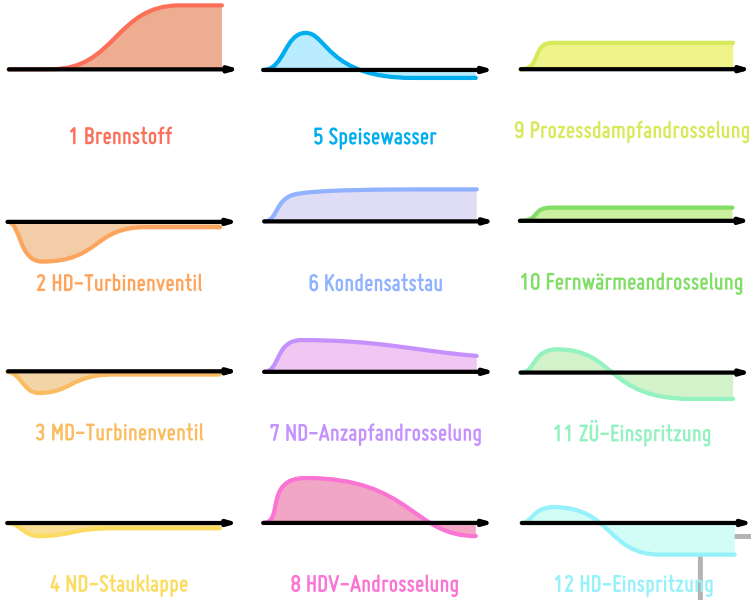
04 Dynamic power plant modelling

Overview of implemented I&C systems



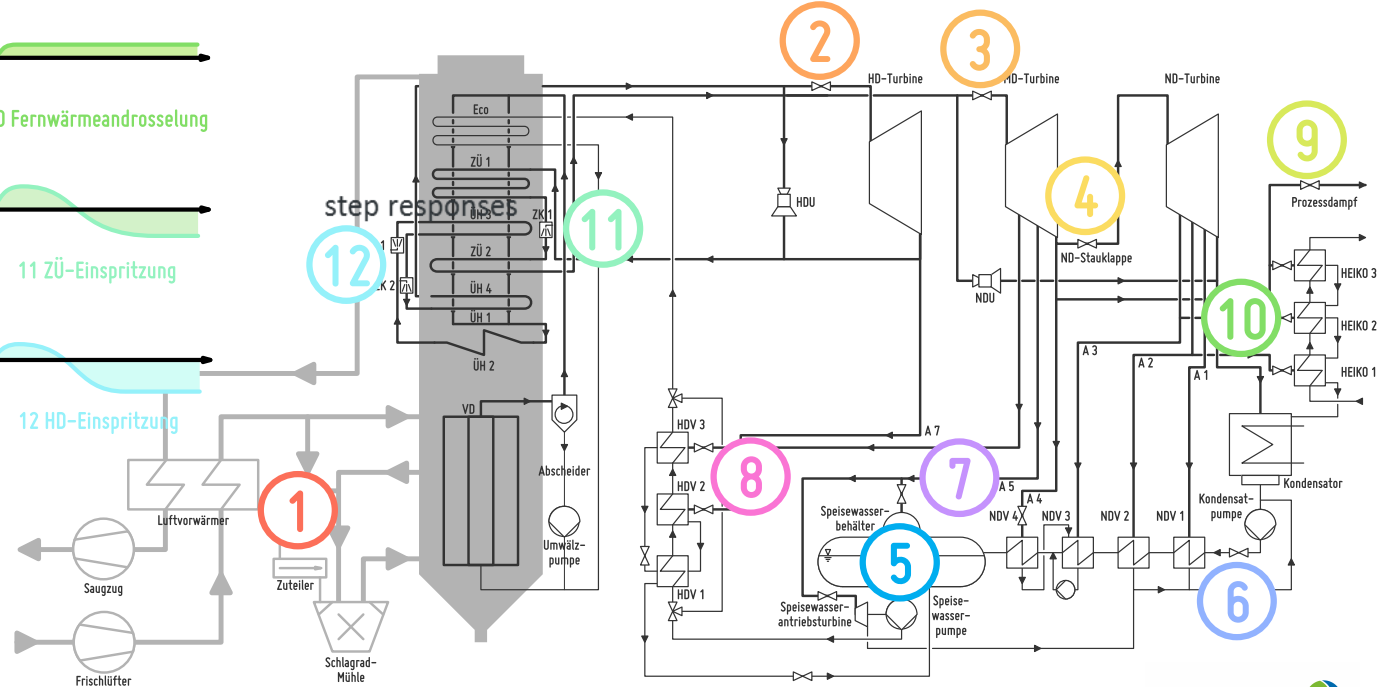
04 Dynamic power plant modelling

Step responses



Step responses :

- Determination of the step responses of the different control interventions
- The load-dependent system dynamics form the basis for further controller design and system optimization.

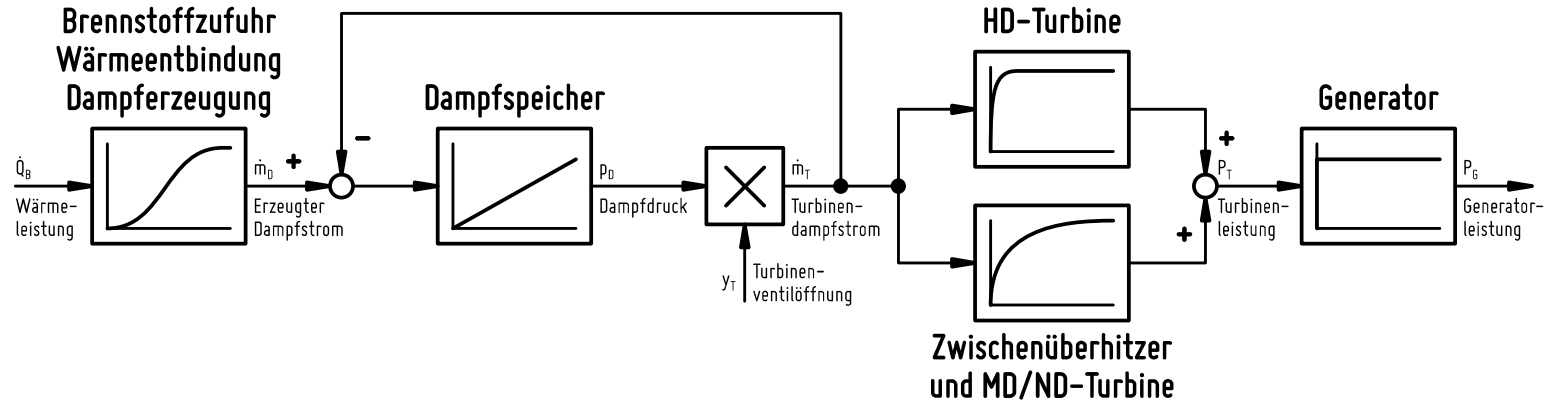


05 Using the model

analyse the I&C System



Scheme of the dynamic processes in a steam power plant



Description Dynamic steam power plant according to VDI/VDE 3508::

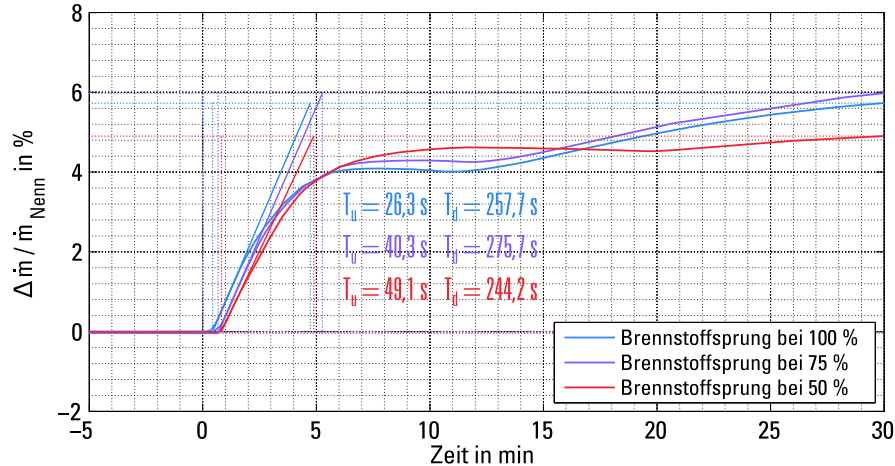
- Sub-process of fuel supply, heat transfer and steam generation, characterized by higher order time behaviour with delay time T_u and compensation time T_g
- Characterization of the steam generator storage capacity by an integrator with a time constant
- the reheater has a storage capacity with a first-order time response

05 Using the model

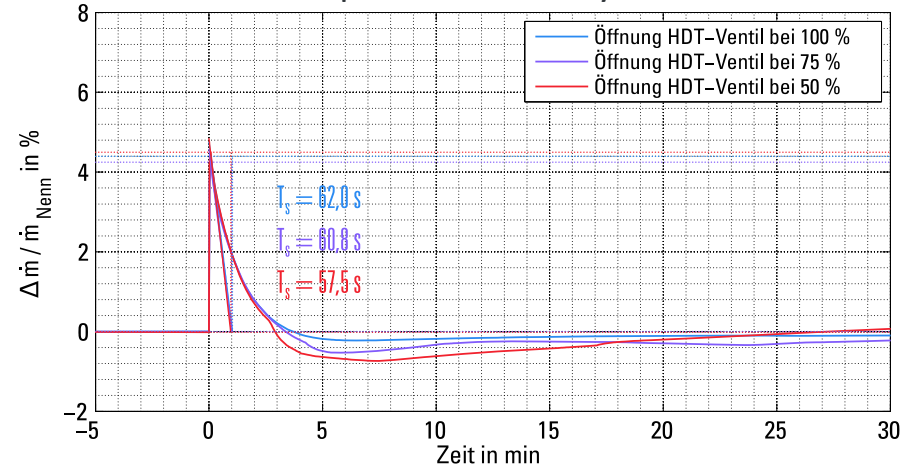
Identifying the time constants



Identifikation Zeitkonstanten Dampferzeugung mit dynamischem Modell



Identifikation Speicherkonstante mit dynamischem Modell



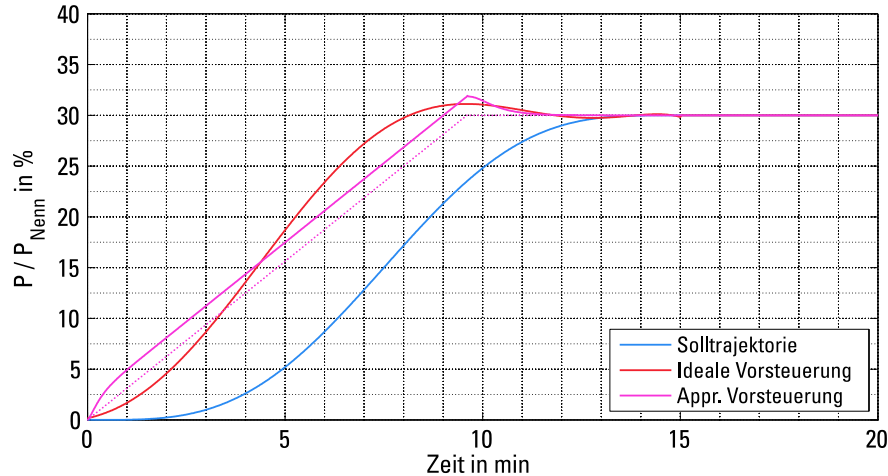
- Step response of the steam quantity to a fuel jump and HP turbine valve opening
- comparable dynamic in full and partial load recognizable
- typical values for the dynamics of steam generation and storage in lignite-fired continuous-flow boilers 30 to 60 s for delay time T_u and 250 s for compensation time T_g
- According to the guideline, 60 to 140 s are typical time constants for the steam storage of the boiler.

05 Using the model

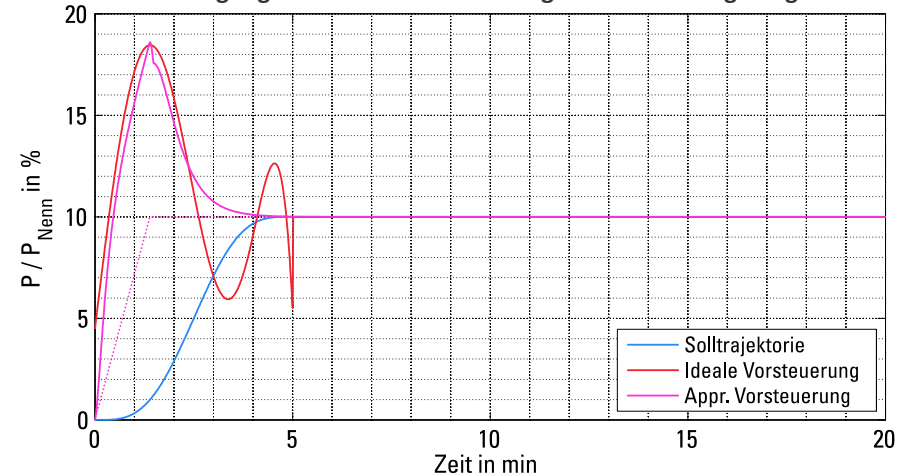
Design Precontrol Timetable change / minute reserve



Auslegung Brennstoff-Vorsteuerung für Fahrplanänderung



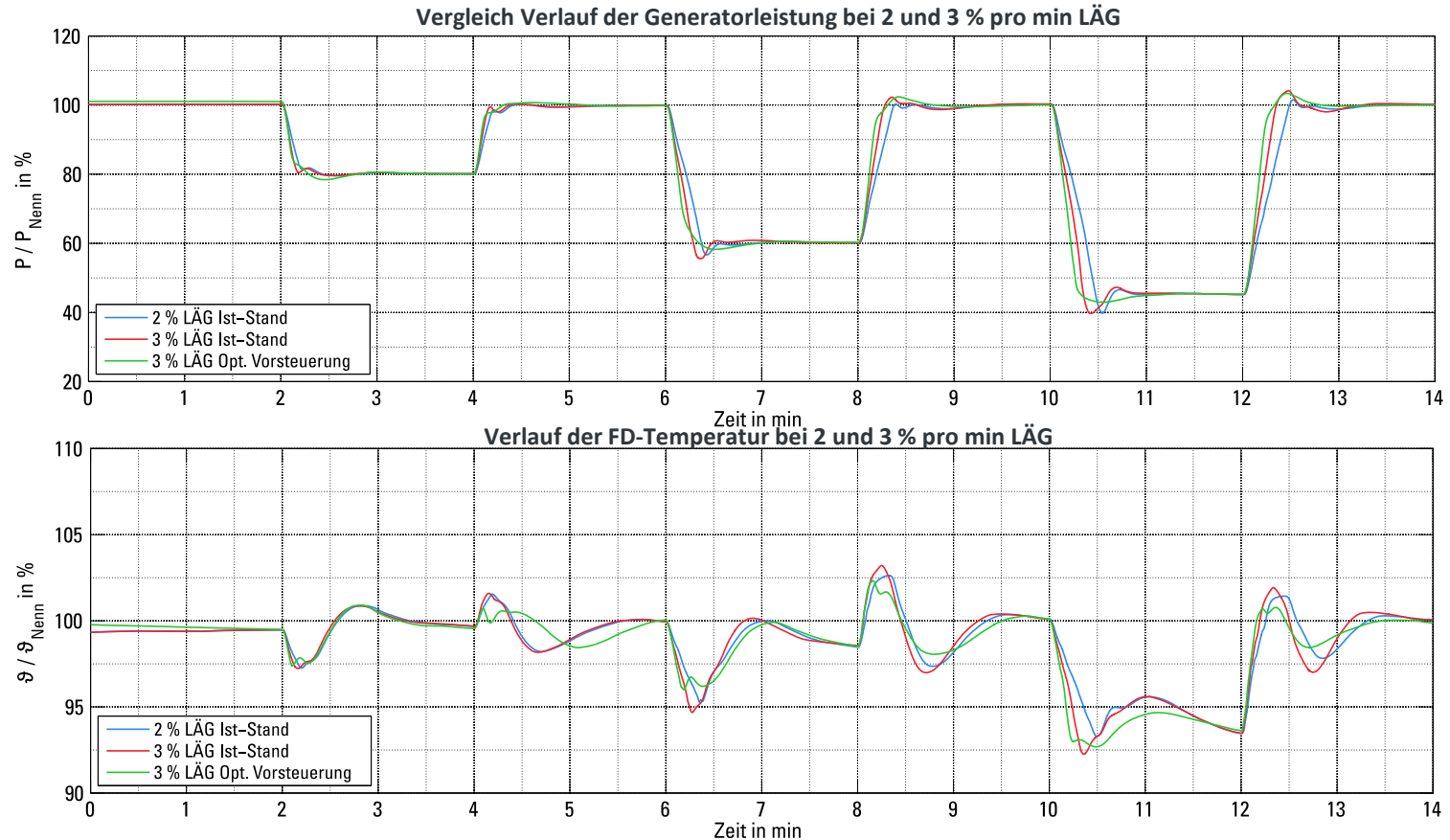
Auslegung Brennstoff-Vorsteuerung für Sekundärregelung



- In the event of a change in the timetable, an increase in performance of 30 % in 15 minutes or 2 % per minute is achieved
- For secondary control Power increase of 10 % in 5 min
- The shorter time of the target trajectory in relation to the time constants of the steam generator requires noticeably more aggressive oversteering than in the case of a timetable change.
- Calculation of an ideal pre-control of the heat output depending on the inertia of the DE and the target trajectory
- Approximation of the ideal feedforward by means of load ramp and overload

05 Using the model

Simulation of the I&C change

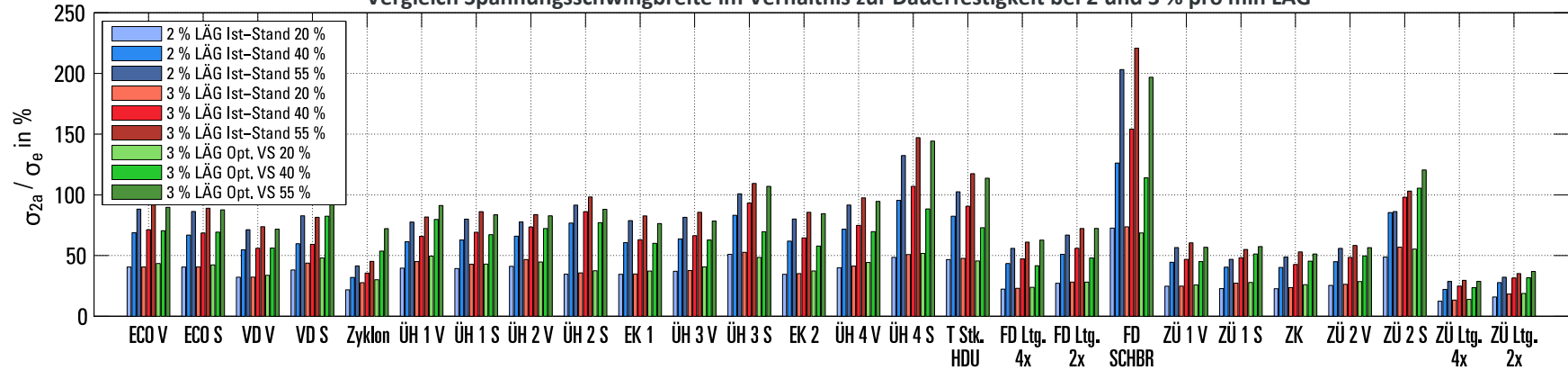


05 Using the model

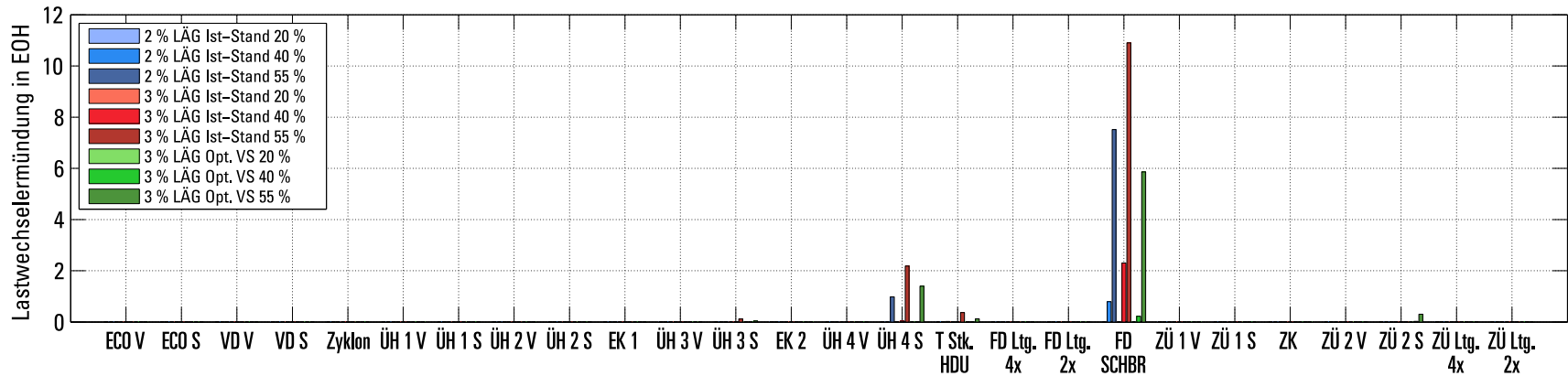
Simulation der leittechnischen Änderung



Vergleich Spannungsschwingbreite im Verhältnis zur Dauerfestigkeit bei 2 und 3 % pro min LÄG



Vergleich Lastwechsellermüdung in äquivalenten Betriebsstunden bei 2 und 3 % pro min LÄG (1 EOH = 1/200.000 der Lebensdauer)





Model Jänschwalde :

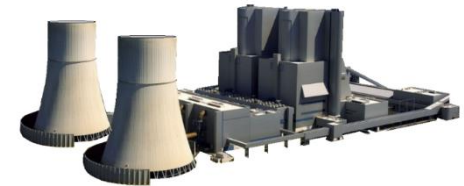
- Model development in cooperation with the University of Rostock 2012-14
- investigation of:
 - Mod. Sliding and fixed pressure operation
 - Increased load change rates with consideration of change exhaustion
 - Provision of system services and potentials of second reserve measures
 - Evaluation of I&C optimizations - block control and steam temperature control
- The results are included in the project "Increase of secondary control power KW JÄW".



KW Jänschwalde

Model Schwarze Pumpe:

- Creation of a dynamic model 2015-17 and parallel performance of stationary and dynamic operating data analyses to identify optimization potentials with the FVTR
 - investigation of :
 - Increased load change rates with consideration of change exhaustion
 - Jump tests and evaluation of load-dependent system dynamics
 - Evaluation of I&C optimizations - Correction of enthalpy setpoint for load increases and partial loads
 - Evaluation of process engineering adaptations - HD step valve
 - Simulation of load shedding with provision of process steam
- Vorstellung der Ergebnisse am Standort Ende Juni



KW Schwarze Pumpe



Model Boxberg Q:

- Start of work in Q2 2018 with FVTR
- Parallel creation of a dynamic operating data analysis
- Project kick-off and presentation of the analysis results at the site at the end of June
- Cooperation with ABB in the mapping of control technology within the WiR project
- Planned completion of model creation in Q 3 2019
- Subsequently, simulation of adapted operating modes and evaluation of process and I&C optimizations



KW Boxberg Q

Langfristige Zielstellung:

- Interlocking of existing tools for comprehensive evaluation of possible measures for plant optimization :
 - Power plant deployment planning model to determine the future operation mode and boundary conditions
 - Stationary operating data analysis with the aid of PGÜ
 - Dynamic operational data analysis using operational measurements and PDN
 - Joint development of a requirement specification for plant optimization in cooperation with the controlling department
 - Analysis of the accounting data of the maintenance with regard to the effects of the adapted driving style

VIELEN DANK FÜR IHRE AUFMERKSAMKEIT!

Jan Koltermann
Abt. Modernisierung & Effektivitätssteigerung



Universität
Rostock



Traditio et Innovatio

